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## **Thermo-kinetic research methods for simple order reactions: Analog curve and characteristic parameter methods**

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### **Abstract**

In order to simplify the thermo-kinetic research method and study faster reactions, two novel thermo-kinetic research methods, namely the thermo-analytical analog curve and characteristic parameter methods, have been proposed in this paper. The general formulae for calculating kinetic parameter  $K_n$  and rate constant  $k_n$  have been derived.

The thermo-kinetics of five reactions with first, second, third, and fractional orders, respectively, have been studied with these methods, and their validity has been verified by the experimental results. © 1997 Elsevier Science B.V.

*Keywords:* Analog thermo-analytical curve method; Characteristic parameter method; Simple order reactions; Thermo-kinetic research method

Based on the fundamental theory of thermo- In this paper, two novel research methods for studykinetics, the dimensionless parameter method of dif- ing slower and faster reactions, the analog thermoferent order reactions had been developed in literature analytical curve and characteristic parameter methods, [1-7], and it can be applied to study slower reactions have been proposed. The formulae for calculating the as well as faster ones when the ratio of the thermo- kinetic parameters and rate constants are very simple analytical curve characteristic data  $a_m^*/A$  is beyond its when these methods are followed. In order to test the critical value. In addition, different order reactions validity of these methods, we have studied the sapohave different forms of the dimensionless parameter infications of ethyl butyrate and ethyl propionate in method. This is inconvenient for the users. In practice, aqueous ethanol and water, respectively, the formation many chemical and biochemical reactions are rapid of hexamethylenetetramine in water, and the polymerand, consequently, it is necessary to develop a thermo- ization of acrylamide. The rate constants calculated by

1. Introduction **1.** Introduction **kinetic research** method applicable to these faster reactions.

the proposed methods are in agreement with those in the literature, and therefore, the analog thermo-analytical curve and characteristic parameter methods \*Corresponding author, were validated.

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### *2.1. The analog thermo-analytical curve equation and the thermo-kinetic characteristic equations of simple order reactions* Inserting Eqs. (3) and (4) into Eq. (1), we have

The thermo-analytical curve for a chemical reaction occurring in a conduction calorimeter is shown in Fig. 1. It varies with the reaction order, the rate Eq. (5) is the characteristic expression of the analog the ratio is the rate thermo-analytical curve. constant and initial concentrations of reactants. How-<br>The peak area of the analog thermo-analytical curve.<br>The peak area of the analog thermo-analytical curve ever, it can be approximately simulated by the follow-<br>is given by  $\frac{1}{\text{ne}}$  peak ing relationship:

$$
\Delta = at e^{-k\beta t} \tag{1}
$$

Eq. (1) is called the analog thermo-analytical curve equation. Therein, k is the cooling constant of a Inserting Eq. (5) into Eq. (6) we have thermo-kinetic system, t the reaction time,  $\Delta$  the peak height at time t,  $\alpha$  and  $\beta$  the analog parameters related to the thermo-kinetic system. When  $t = 0$ ,  $\Delta = 0$ , and Let the peak area and the characteristic peak height of when  $t \to \infty$ ,  $\Delta \to 0$ ; thus, it is clear that the analog the analog thermo-analytical curve be equal to those of thermo-analytical curve respectively. From

$$
\frac{d\Delta}{dt} = \alpha (1 - k\beta t) e^{-k\beta t}
$$
 (2)

At  $t = t_m$ ,  $d\Delta/dt = 0$ , and  $\Delta = \Delta_m$ , from Eq. (2) we Inserting Eq. (7) into Eq. (3), we obtain the cooling have

$$
\beta = 1/(kt_m) \tag{3}
$$



matic).  $K_n$  being the kinetic parameter.

**2. Theory and method** At  $t=t<sub>m</sub>$ , from Eq. (1), and taking into account Eq. (3), we have

$$
\alpha = e\Delta_{\rm m}/t_{\rm m} \tag{4}
$$

$$
\Delta = t/t_{\text{m}\Delta_{\text{m}}}e^{(1-t/t_{\text{m}})}\tag{5}
$$

$$
\Delta = at e^{-k\beta t}
$$
 (1) 
$$
A = \int_0^{+\infty} \Delta dt
$$
 (6)

$$
t_{\rm m} = A/(\mathrm{e}\Delta_{\rm m})\tag{7}
$$

the real thermo-analytical curve, respectively. From tions of the real thermo-analytical curve. Eq. (7),  $t_m$  can be calculated with A and  $\Delta_m$  of the real Differentiating Eq. (1) with respect to t, we have thermo-analytical curve. From Eqs. (5) and (7), it can be seen that the analog thermo-analytical curve can be determined according to the real thermo-analytical curve.

constant of the thermo-kinetic system:

$$
k = e\Delta_{\rm m}/(\beta A) \tag{8}
$$

Based on the fundamental theory of thermo-kinetics [1], the thermo-kinetic characteristic equations of simple-order reactions are given by

$$
\Delta_{\mathsf{m}}/A = \varphi(K_{\mathsf{n}}, t_{\mathsf{m}}) \tag{9}
$$

$$
a_m^*/A - \Delta_m/(kA) = \psi(K_n, t_m)
$$
 (10)

Here, A,  $\Delta_{\rm m}$ ,  $t_{\rm m}$  and  $a_{\rm m}^{*}$  are the thermo-analytical curve characteristic data representing the total area,  $\overrightarrow{p}$  maximum peak height, time corresponding to  $\Delta_{\rm m}$  and the peak area after  $t_m$  of a thermo-analytical curve, respectively, (see Fig. 1);  $\varphi(K_n, t_m)$  and  $\psi(K_n, t_m)$  are  $t_n$  functions with respect to  $K_n$  and  $t_m$  which reflect the kinetic characteristics of the thermo-kinetic system Fig. 1. Thermo-analytical curve of a chemical reaction (sche- and have different forms for different order reactions,

$$
\Phi_{\mathsf{m}} = a_{\mathsf{m}}^*/A - \Delta_{\mathsf{m}}/(kA) \tag{11} \qquad \qquad \Phi_{\mathsf{m}} = a_{\mathsf{m}}^*/A - \beta/\mathsf{e} \tag{13}
$$

$$
\Phi_{\mathbf{m}} = \psi(K_{\mathbf{n}}, t_{\mathbf{m}}) \tag{12}
$$

ing  $\Phi_m$ ; hence, two thermo-kinetic research methods Table 1) **can be derived, as described in the following sections.** 

### *2.2. Analog thermo-analytical curve method*

**Table** 1 **Formulae for calculating K. and** kn

Let we have

$$
\Phi_{\mathsf{m}} = a_{\mathsf{m}}^* / A - \beta / e \tag{13}
$$

Combining Eq. (11) with Eq. (10), we have From Eq. (12) and corresponding rate equations of **different order reactions, the formulae for calculating** kinetic parameters  $K_n$  and rate constants  $k_n$  for dif-According to Eq. (11), there are two ways of calculat- ferent order reactions can be obtained (shown in

### *2.3. Characteristic parameter method*

Another way to calculate  $\Phi_{\rm m}$  is to calibrate the One way to calculate  $\Phi_m$  is to determine the cooling cooling constant according to an already described constant with Eq. (8). Inserting Eq. (8) into Eq. (11), procedure [8]. From Eqs. (9) and (12) and correspond-

rormulae for calculating $K_n$ and $K_n$			
Reaction type	$K_n$ <sup>a</sup>	$K_n$ <sup>b</sup>	$k_n$
First-order reaction	$K_1 = -\frac{1}{t_m} \ln \Phi_m$	$K_1 = \frac{\Delta_m/A}{\Phi}$	$k_1 = K_1$
Second-order reaction with unequal concentrations	$K_2^* = \frac{1}{t_m} \ln \left[ \frac{1 + (r - 1)/\Phi_m}{r} \right]$ $K_2^* = \frac{\Delta_m/A}{\Phi_m + \Phi^2/(r-1)}$		$k_2 = K_2^*/(A_0 - B_0)^c$
nth-order reaction with equal concentrations	$K_n = \frac{1}{(n-1)t_m} \left[ \Phi_{m}^{(1-n)} - 1 \right]$ $K_n = \frac{\Delta_m/A}{\Phi^n}$		$k_n = K_n/C_0^{(n-1)}$ c
Reaction with fractional-order 1/2	$K_{1/2} = \frac{2}{t_{-}} \left[ 1 - \Phi_{m}^{1/2} \right]$	$K_{1/2} = \frac{\Delta_{\rm m}/A}{\Phi_{\rm m}^{-1/2}}$	$k_{1/2} = K_{1/2} C_0^{1/2}$
3/2	$K_{3/2} = \frac{2}{t_m} [\Phi_{m}^{-1/2} - 1]$	$K_{3/2} = \frac{\Delta_{\rm m}/A}{\Phi^{3/2}}$	$k_{3/2} = K_{3/2} C_0^{-1/2}$
5/2	$K_{5/2} = \frac{2}{3t} [\Phi_{\rm m}^{-3/2} - 1]$	$K_{5/2} = \frac{\Delta_{\rm m}/A}{\Phi_{\rm m}^{5/2}}$	$k_{5/2} = K_{5/2} C_0^{-3/2}$

**a Analog thermo-analytical curve method.** 

<sup>c</sup> A<sub>0</sub>, B<sub>0</sub>, C<sub>0</sub> are the initial concentrations of reactants;  $r = A_0/B_0 (> 1)$ 

**b Characteristic parameter method.** 

ing rate equations of different order reactions, the All the reagents of the above reactions were be obtained (shown in Table l). water.

From Table 1, it is seen that the mathematical models of our two novel thermo-kinetic research methods, in the present paper, are very simple, espe- *3.2. Apparatus*  cially for the nth-order reactions with equal concentrations of reactants there are general mathematical All the thermo-analytical curves of the above-menmodels. The models is tioned reactions were measured with a twin conduc-

Table 2

### *3.1. Reactions and reactants*

In order to test the validity of the analog thermoanalytical curve and characteristic parameter methods, 4. Results and discussion the thermo-kinetics of five different order reactions as shown below, have been studied. *4.1. Verification of the analog thermo-analytical* 

- Pseudo-first-order reaction: saponification of ethyl
- trations: saponification of ethyl propionate in
- 
- tramine at 15°C.
- **Fractional-order reaction: the polymerization of given below Fractional-order reaction: the polymerization of given below** acrylamide at 30°C. 6HCHO + 4NH<sub>3</sub>  $_{\rm 6HCHO + 4NH_3}$   $_{\rm 6HCHO + 4NH_3}$

formulae for calculating kinetic parameters,  $K_n$ , and analytically pure. The mixed solvents were prepared rate constants  $k_n$  for different order reactions can also from analytically pure ethanol and deionized

tion calorimeter, described in detail in the previous article [8]. In an earlier paper, we have described a 3. Experimental method for measuring the cooling constant of a thermo-kinetic system [9].

# *curve and characteristic parameter methods.*

butyrate in aqueous ethanol solvent at 30°C.<br>Second-order reaction with equal reactant concen-<br> $R_n$  and  $k_n$ <br> $R_n$  and  $k_n$  $\text{in Table 1}$  and Eq. (11), or Eqs. (7) and (13), the rate water at 25<sup>°</sup>C. curve characteristic data  $a_m^*$ ,  $\Delta_m$  and A. The results of **•** Second-order reaction with unequal reactant con-<br>the above-mentioned different order reactions are<br>centrations: saponification of ethyl benzoate in<br> $\mathbf{r}$ centrations: superinteation of  $\sum_{i=1}^{\infty}$  centrations in listed in Tables 2–6, in which,  $K_1^* = K_1$  for a pseudo-first-order reaction,  $k_{3/2} = K_2 C_0^{1/2}$  (Na<sub>2</sub>SO<sub>3</sub>) Third-order reaction: the reaction of formaldehyde for the polymerization of acrylamide. The reaction with ammonia in water to form hexamethyleneteequation of formaldehyde with ammonia in water is

$$
6HCHO + 4NH_3 \stackrel{\kappa_3}{\rightarrow} (CH_2)_6N_4 + 6H_2O
$$





<sup>a</sup> Results calculated according to the analog thermo-analytical curve method.

**b Results calculated according to the characteristic parameter method.** 

<sup>c</sup> Results calculated according to the dimensionless parameter method.





<sup>a</sup> Same as in Table 2.

b Same as in Table 2.

 $\degree$  Same as in Table 2.

Table 4

Saponification of ethyl benzoate at 25°C (Solvent: 50% (w/w) E<sub>t</sub>OH-H<sub>2</sub>O;  $k=1.96\times10^{-3}$  s<sup>-1</sup>)

$C_0$ (ester)/ $(mod l^{-1})$	$C_0$ (NaOH)/ $(mod l^{-1})$		$\Delta_{\rm m}$ / mm	$a_m^* \times 10^{-5}$ / (mm s)	$A \times 10^{-5}$ / (mm s)		$k_2 \times 10^{3}$ / $(1 \text{ mol}^{-1} \text{ s}^{-1})$	
0.300	0.100		67.8	2.19	2.66	1.38 <sup>a</sup>	1.37 <sup>b</sup>	1.35 <sup>c</sup>
0.500	0.100		135	2.82	3.58	1.30	1.38	1.37
0.350	0.0500		89.2	2.38	2.90	1.37	1.39	1.31
0.397	0.0460	8.63	95.0	2.39	2.95	1.30	1.31	1.30
0.451	0.0464	9.72	76.5	1.75	2.29	1.36	1.30	1.32
					Average:	1.34	1.35	1.33
					Ref. [12]:	1.33		

 $\overline{\text{a}$  Same as in Table 2.

**b** Same as in Table 2.

c Same as in Table 2.

Table 5

Formation of hexamethylenetetramine at 15°C (Solvent: H<sub>2</sub>O;  $k=1.83\times10^{-3}$  s<sup>-1</sup>)

$C_0$ (HCHO)/ $(mod 1^{-1})$	$C_0$ (NH <sub>3</sub> )/ $(mod 1^{-1})$	$\Delta_{\bf m}$ mm	$a_m^* \times 10^{-5}$ / (mm s)	$A \times 10^{-5}$ / (mm s)		$k \times 10^2$ / $(1^2 \text{ mol}^{-2} \text{ s}^{-1})$	
0.0600	0.0400	37.6	1.73	1.95	2.60 <sup>a</sup>	2.80 <sup>b</sup>	2.90 °
0.0600	0.0400	34.9	1.66	1.86	2.46	2.64	2.71
0.0540	0.0360	27.2	1.57	1.76	2.50	2.51	2.76
0.0540	0.0360	27.5	1.49	1.68	2.73	2.77	2.96
0.0540	0.0360	24.5	1.44	1.63	2.56	2.52	2.80
				Average:	2.57	2.65	2.79
				$[13]$ :	2.84 <sup>d</sup>		

<sup>a</sup> Same as in Table 2.

b Same as in Table 2.

<sup>c</sup> Same as in Table 2.

d Obtained from the half-life in [13].

$$
t = 0 \t 6C_0 \t 4C_0 \t 0 \t 0
$$
  
\n
$$
t = t \t 6(C_0 - x) \t 4(C_0 - x) \t x \t 6x
$$
  
\n
$$
\frac{dx}{dt} = 144(C_0 - x)^3
$$

Thus, the kinetic parameter of this reaction is  $K_3=144k_3 C_0^2$ .

From Tables 2-6, it can be seen that the rate constants of different order reactions calculated with our  $dt = \frac{1}{1 + \sqrt{6}}$   $\frac{d}{dx}$  two novel methods are in agreement with those in the

Table 6 Polymerization of acrylamide at 30°C (Solvent: H<sub>2</sub>O;  $k=1.88\times10^{-3}$  s<sup>-1</sup>)

$C_0(A)$ $(mod 1^{-1})$	$C_0$ (B) $\times 10^4$ / $(mod 1^{-1})$	$\Delta_{\rm m}$ / mm	$a_M^* \times 10^{-5}$ / (mm s)	$A \times 10^{-5}$ / (mm s)	$k_{3/2} \times 10^4$ / $(1^{1/2} \text{ mol}^{-1/2} \text{ s}^{-1})$		$k_2 \times 10^{2}$ / $(1 \text{ mol}^{-1} \text{ s}^{-1})$		
0.2017	1.651	35.8	5.94	6.39	1.41 <sup>a</sup>	1.47 <sup>b</sup>	1.10 <sup>a</sup>	1.15 <sup>b</sup>	1.13 <sup>c</sup>
0.4946	6.447	78.2	4.85	5.64	2.94	2.83	1.16	1.11	1.15
0.5675	6.050	85.8	5.13	5.78	2.65	2.71	1.08	1.10	1.07
0.5974	6.175	95.0	5.50	6.38	2.86	2.78	1.15	1.12	1.14
0.3432	3.295	74.0	6.84	7.46	2.05	2.11	1.14	1.16	1.13
0.3448	4.606	76.0	6.05	6.68	2.43	2.49	1.13	1.15	1.13
0.3473	5.226	77.2	5.61	6.17	2.63	2.74	1.15	1.19	1.15
						Average:	1.13	1.14	1.14
						[7]:	1.13		

<sup>a</sup> Same as in Table 2.

b Same as in Table 2.

c Same as in Table 2.

literature and, therefore, the analog thermo-analytical *4.3. The comparison of the analog thermo-analytical*  curve and characteristic parameter methods are *curve with the real thermo-analytical curve*  believed to be correct.

From Table 1, it can be seen that the key to calculate the validity of Eq.  $(5)$  for simulating the real thermothe rate constants accurately lies in the determination analytical curve has been verified. of the precise value of  $\beta$ . According to our experimental results, when the initial rate of a studied reaction is faster, the value of  $\beta$  is larger, otherwise,  $\alpha$  4.4. Comparison of the analog thermo-analytical when the initial rate of a studied reaction is slower, the *curve and characteristic parameter methods*  value of  $\beta$  is smaller. Generally speaking, when the *with the dimensionless parameter method.* initial rate of a reaction  $>10^{-4}$  mol  $1^{-1}$ s <sup>-1</sup>, the value of  $\beta$  turns out to 1; however, when the initial rate of a From Tables 2–6, we can see that the rate constants studied reaction is <10<sup>-4</sup> mol 1<sup>-1</sup>s<sup>-1</sup>, the value of  $\beta$  is of the slow reactions calculated with the analog 2/3. When the initial rate is  $\sim 10^{-4}$  mol  $1^{-1}$  s<sup>-1</sup>, we thermo-analytical curve and characteristic parameter can change the initial concentrations of reactants to methods and the dimensionless parameter method are make it far smaller than or larger than in agreement with those in the literature, but the  $10^{-4}$  mol  $1^{-1}$  s<sup>-1</sup>, so that the experimental results will dimensionless parameter method cannot be applied be credible, to faster reaction (see Table 3). The reason is that the

determined heuristically. First, the rate constants can methods only require the thermal change process to be calculated with two values of  $\beta$ , namely 2/3 and 1; satisfy the Tian equation, but the dimensionless parathen the initial rate can be calculated. With this initial meter method not only requires the thermal change rate, the value of  $\beta$  can be determined with the above- process to satisfy the Tian equation, but also stipulates mentioned method. The ratio  $a_m^*/A$  must be greater than the critical

The analog thermo-analytical curves of saponification of ethyl benzoate and ethyl propionate are shown *4.2. Determination of*  $\beta$  *in the analog thermo-* in Figs. 2 and 3, respectively. From the two figures, we *analytical curve method* can see that the real thermo-analytical curve can reasonably be well simulated by the analog thermo-For a thermo-analytical curve,  $t_m$  is determinate. analytical curve for a slower or faster reaction. Thus,

For an unknown reaction, the value of  $\beta$  can be thermo-analytical curve and characteristic parameter



Fig. 2. Saponification of ethyl benzoate: (a) - real thermo-analytical curve (Table 4 No. 1); (b) - analog thermo-analytical curve  $(\Delta = 0.0470te^{1-t/1443}, \beta = 2/3).$ 



Fig. 3. Saponification of ethyl propionate: (a) - real thermo- [7] Xian-Cheng Zeng, Qing-Hua Liu, Yu Deng and Gan-Zuo Li, analytical curve (Table 3, No. 1); and (b) – analog thermo-<br>analytical curve  $(\Delta = 0.192 t e^{1-t/356}, \beta = 1)$ .<br>Fig. Yinn, Chang, Chang,

value obtained by this method. Therefore, the analog [9] Xian-Cheng Zeng, Yuan-Qing Zhang, Qi-Shang Hu and Anthermo-analytical curve and characteristic parameter Ming Tian, Acta Chimica Sinica, in press. methods have a wider applicable range than the [10] A.A. Smith and H.S. Levenson, J. Am. Chem. Soc., 61 (1939) dimensionless parameter method. Thus, the two for-<br>mer methods can be more widely used to study [11] C.H. Bamford and C.F.H. Tipper, Ester Formation and mer methods can be more widely used to study [11] C.H. Bamford and C.F.H. Tipper, Ester Formation and <br>Hydrolysis and Related Reactions, Elsevier, New York, chemical and biochemical reactions.

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